

AMENDMENTS TO THE CLAIMS

This listing of claims will replace all prior versions, and listings, of claims in the application.

Listing of Claims

1-12. (Cancelled).

13. (Currently Amended) A TEMPO-free process of cleaning a polymer membrane filter containing residues from filtering beverages, the residues containing water-insoluble proteins and/or polyphenols attached to the filter and polysaccharides, comprising contacting the protein and/or polyphenol containing residues with a solution containing a peroxide compound in the presence of a transition metal selected from manganese and iron, by back-flushing, wherein said peroxide is used at a concentration within the range from 200 to 5000 2000 ppm.

14-15. (Cancelled).

16. (Previously Presented) The process according to claim 13, wherein the transition metal is complexed with a polyamine.

17. (Previously Presented) The process according to claim 13, wherein the peroxide is hydrogen peroxide.

18. (Previously Presented) The process according to claim 13, wherein the peroxide is a peracid.

19. (Cancelled).

20. (Currently Amended) A TEMPO-free process of cleaning a polymer membrane filter containing residues from filtering beverages, the residues containing water-insoluble proteins and/or polyphenols attached to the filter and polysaccharides, comprising contacting the protein and/or polyphenol containing residues with a solution containing a hypohalous acid by back-flushing, wherein said hypohalous acid is used at a concentration within the range from 200 to ~~5000~~ 2000 ppm.

21. (Previously Presented) The process according to claim 20, comprising contacting the protein and/or polyphenol containing residues with an alkaline solution prior to said contacting with said solution containing a hypohalous acid.

22. (Previously Presented) The process according to claim 21, wherein the alkaline solution has a pH between 11 and 14.

23. (Cancelled).

24. (Previously Presented) The process according to claim 13, wherein said transition metal is used at a concentration within the range from 1 to 50 ppm.

25. (Cancelled).

26. (Previously Presented) The process according to claim 13, wherein the back-flush is performed at a rate of 0.5-100 liters of the solution per h per m² of filter surface.

27. (Previously Presented) The process according to claim 20, wherein the back-flush is performed at a rate of 0.5-100 liters of the solution per h per m² of filter surface.